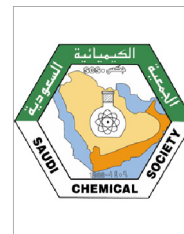




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ORIGINAL ARTICLE

Green synthesized SiO₂@OPW nanocomposites for enhanced Lead (II) removal from water

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KEYWORDS

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Adsorption isotherms;
Adsorption kinetics

Abstract The orange peel waste (OPW) was chemically spiked with silica nanospheres, to develop a novel, nanocomposite (SiO₂@OPW) with enhanced adsorption capacity for heavy metals. The dispersion of silica nanospheres into orange peel waste was confirmed by XRD, FTIR, TEM, SEM and EDX. Adsorption of Pb²⁺ ions onto SiO₂@OPW was studied in batch mode under varying process conditions such as pH, metal concentration, contact time and adsorbent dosage. The maximum adsorption capacity for OPW and SiO₂@OPW was 166.7 mg/g and 200.0 mg/g, respectively calculated employing the Langmuir isotherm model. The kinetic data followed pseudo second order and intraparticle diffusion models. The maximum removal of Pb²⁺ ions was at pH = 6.0, adsorbent dosage = 0.02 g/L and contact time 60 min. Regeneration and reusability of SiO₂@OPW was studied for five cycles. Owing to reusability and high adsorption capacity, SiO₂@OPW nanocomposites may be considered as a promising adsorbent for the removal of heavy metals from water and wastewater.

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1. Introduction

During the past decades, heavy metals have emerged as a major inorganic pollutant and threat to natural environment and human health. The only solution to protect the

environment and human health is their removal from metal laden wastewater before discharging them into aqueous streams. These metal ions, primarily originate from electroplating, mining & ore processing, paint, chemicals and fertilizer industries and metal surface treatment processes (Lawal et al., 2017; Charles et al., 2017; Miranda et al., 2016). Lead is more toxic as compared to several other heavy metals like copper, manganese, zinc and cobalt. Exposure to Pb may cause abdominal pain, neonatal deaths, sterility, damages the nervous system, liver and kidney and affects the process of hemoglobin synthesis, porphyrin metabolism by forming complexes with oxo-groups in enzymes (Charles et al., 2017; Miranda et al., 2016; Rajput et al., 2015). Therefore, it is essential to remove Pb from wastewater before being released into aqueous bodies.

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Several conventional technologies are in use for Pb removal from. These technologies include chemical precipitation, redox approach, ion exchange, electrolysis, membrane separation and adsorption. Amongst these, adsorption is more reliable and promising owing to its efficiency, local availability of adsorbents, operational simplicity, cost effectiveness and regeneration potential of the adsorbents (Musico et al., 2013; Kumar et al., 2014; Joshi et al., 2018; Thitame and Shukla, 2017). Nanoparticles are a new generation of materials emphasized for the environmental remediation due to their unique properties including large surface area, small particle size, pore size, surface charge, thermal stability, magnetic property, chemical inertness and biocompatibility (Ahmed et al., 2015). In yesteryears, several studies have reported the removal of Pb from water and wastewater using nanomaterials. Some of the tested nanomaterials are cross-linked melamine based polyamine/CNT composites (Hamouz et al., 2017), dispersible magnetic chitosan/graphene oxide composites (Fan et al., 2013), EDTA-Fe₃O₄ functionalized with SiO₂ via silanization reaction between N-(trimethoxysilylpropyl) ethylenediamine triacetic acid (Yu et al., 2016). Although these materials are capable to remediate the Pb containing water and wastewater. But it is a challenge to prepare new materials (adsorbents) better in terms of efficiency, environment friendly and cost effective at commercial scale. Various low cost bioadsorbents have been investigated, such as cellulose waste, sawdust, palm-fruits, orange peel, sunflower waste etc. Undoubtedly, these adsorbents are economical and available on large scale but they possess low adsorption capacity. Recently attention has been paid to synthesize nanobioadsorbents to improve the adsorption capacity as well as large availability of adsorbent. That is, low cost agricultural waste is modified into nanoscale adsorbents by various physical or chemical techniques. In this study, a novel low cost nanoadsorbent is developed by chemically modified orange peel waste and evaluated its potential as non-adsorbent for the removal of Pb²⁺ ions from aqueous streams. Over the past years, the pristine orange peel has been used to remove metal contaminants of water systems. In this study, silica has been used as a coating material to explore the surface functionality and further enhancing adsorption performance of orange peel waste. Also, comparative adsorption of Pb by pristine orange peel waste (OPW) and silicated orange peel waste (SiO₂@OPW) has been investigated.

2. Experimental section

2.1. Reagents and materials

Orange peels were collected from a food processing industry, India. All other reagents were AR grade and used as such without further purification. The experimental solutions were prepared in double distilled water.

2.2. Synthesis and preparation of the adsorbent

2.2.1. Preparation of dried biomass of orange peel waste

Orange peels were collected from a fruit & vegetable processing industry, washed with double distilled water and dried in oven at 100 °C for 24 h. After that, crushed and sieved through 1.40 mm size sieve and kept in a muffle furnace at 250 °C for

12 h. The powder so obtained was stored in plastic containers for further use.

2.2.2. Preparation of SiO₂ nanoparticles

SiO₂ nanoparticles were prepared by modified Stobber method (Park et al., 2002). 5 mL tetraethoxysilane was added to the absolute ethanol-water 2:1 (v/v) mixture under sonication bath. Then 20 mL of liquor ammonia was dropped slowly into the reaction mixture. The obtained white gel was centrifuged, washed with deionized water and dried in oven at 100 °C for 4 h. Finally fine white nanopowders of SiO₂ nanoparticles was obtained.

2.2.3. Preparation of silicated orange peel waste (SiO₂@OPW) nanocomposites

3.0 g of prepared SiO₂ nanoparticles were dissolved in ethanol-water (1:1) mixture with continuous magnetic stirring at room temperature. Then 15 g of orange peel powder was dispersed in the above reaction mixture. The suspension was stirred for 90 min. and finally transferred to sonication bath for 4 h. The final product SiO₂@OPW was collected by centrifugation, washed and calcined at 200 °C in the muffle furnace.

2.3. Characterization of nanoparticles

The FTIR spectrum was used to identify the functional groups. The IR spectrum of samples was recorded on SHIMADZU IR AFFINITY-I FTIR spectrophotometer using KBr powder. The crystallinity and crystal structure of SiO₂, OPW and SiO₂@OPW were analyzed using X-ray diffraction (XRD). XRD patterns of the samples were recorded at room temperature using a Rigaku Miniflex-II diffractometer with Cu K_α radiation in the 2θ range (20–80°) at a scanning rate of 2°/min. Concentration of Pb²⁺ metal ions in solution was determined by atomic absorption spectrophotometer (AAS). The surface morphology, textural structure and elemental composition of samples were obtained by scanning electron microscope (SEM) and energy-dispersive X-ray spectroscopy

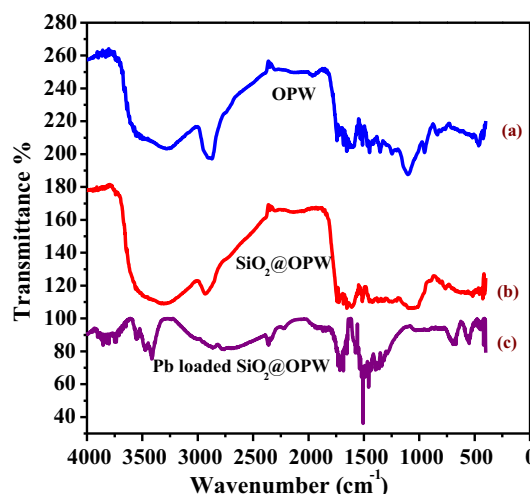


Fig. 1 (a–c) FT-IR spectrum of OPW, SiO₂@OPW and Pb loaded SiO₂@OPW.

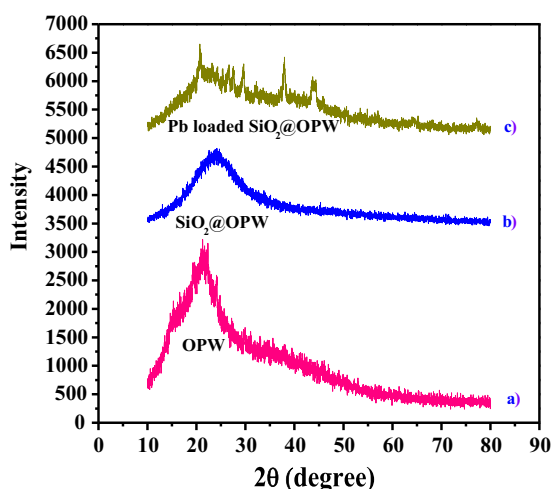


Fig. 2 (a–c) XRD patterns of OPW, SiO₂@OPW and Pb loaded SiO₂@OPW.

(EDX) using Merlin Compact 6073 Scanning Electron Microscope (Carl Zeiss, Germany). Transmission electron

microscopy was done to determine the particle size of SiO₂@OPW by Morgagni 268D (Fei Electron Optics, India).

2.4. Adsorption methods

A stock solution of Pb²⁺ ions (1000 ppm) was prepared in double distilled water using lead nitrate. The adsorption of Pb²⁺ was studied in batch mode experiments under various process conditions like pH, time, concentration, adsorbent dose and adsorbate concentration. Adsorption of Pb²⁺ ions was carried out by shaking known volume of Pb²⁺ solution at constant speed of 180 rpm in a shaker for predetermined time period and then adsorbent was separated by centrifugation. After that, supernatant was used to quantify concentration of Pb²⁺ after the adsorption using Atomic Absorption Spectrophotometer (GBC SensAA). The pH of the solution was adjusted using 0.1 M HCl and 0.1 M NaOH.

The amount of Pb²⁺ ions adsorbed and removal percentage were calculated by the following equations;

$$\text{Metal removal(\%)} = \frac{(C_o - C_e)}{C_o} \times 100 \quad (1)$$

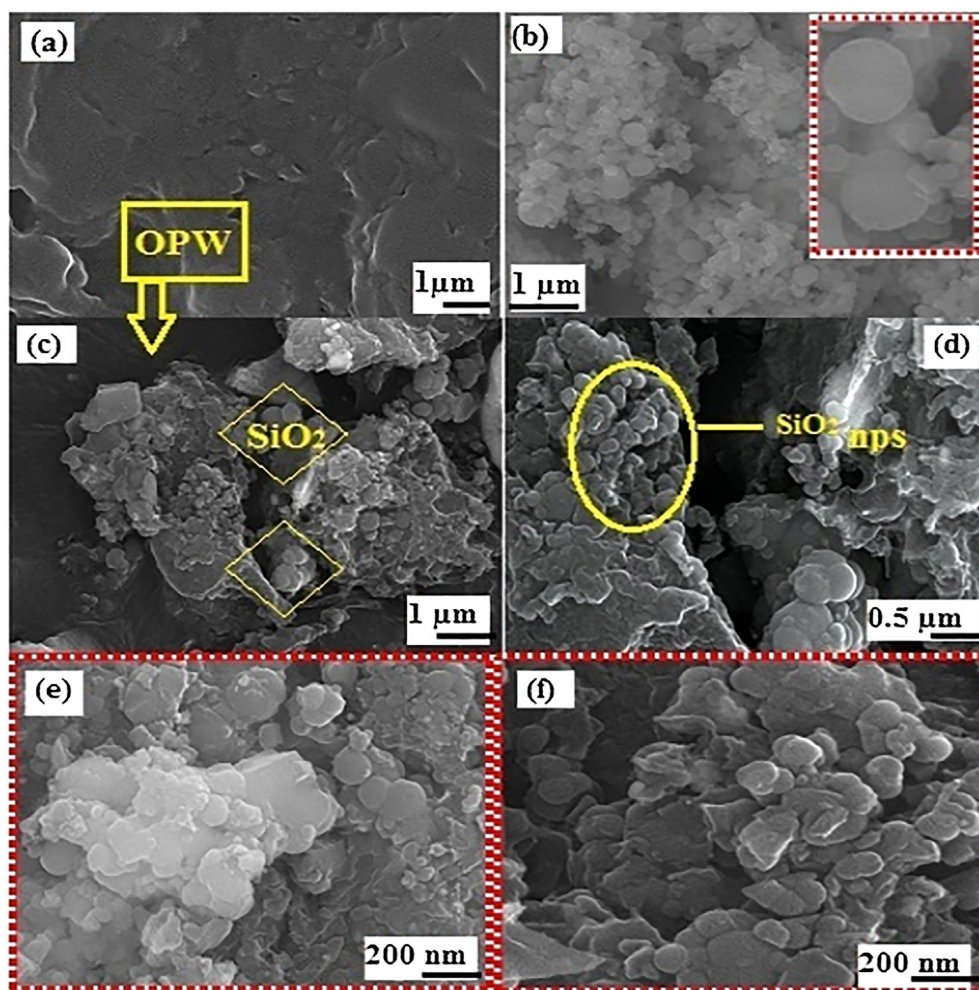


Fig. 3 (a–f) SEM images of (a) OPW (b) SiO₂ and (c–f) SiO₂@OPW.

$$\text{Adsorption capacity}(q_e) = \frac{(C_0 - C_e)V}{m} \quad (2)$$

where C_0 (mg/L) and C_e (mg/L) are the initial and equilibrium concentration of metal ions, respectively, q_e (mg/g) is the amount of Pb^{2+} ions adsorbed onto the adsorbent at equilibrium, V (L) is the volume of solution and m (g) is the mass of adsorbent.

3. Results and discussion

3.1. Characterization of adsorbents

$\text{SiO}_2@\text{OPW}$ nanocomposites were characterized employing various techniques including FTIR, XRD, SEM, EDX and HRTEM.

FTIR spectra of OPW and $\text{SiO}_2@\text{OPW}$ and Pb^{2+} ions loaded $\text{SiO}_2@\text{OPW}$ is shown in Fig. 1. The typical absorption band at $3200\text{--}3488\text{ cm}^{-1}$ in the FTIR spectrum of OPW may be attributed to —OH groups of carbohydrates, pectin and lignin type polymeric compounds (Fig. 1a). The absorption peak at 2935 cm^{-1} is corresponds to C—H symmetric and asymmetric vibrations and peaks at 1735 cm^{-1} is attributed to carboxylic groups (COOH and COOCH_3) (Li et al., 2015; Mafra et al., 2013). The intense peaks appeared at $\sim 1435\text{ cm}^{-1}$ are due to C—H bending vibrations. The signal appeared at 1045 cm^{-1} is due to (C—OH/C—OR) stretching vibrations (Fig. 1a). That absorption peak is becoming somewhat broader in Fig. 1b and almost disappears in Fig. 1c. It may be attributed to the blending of Si—O stretching vibrations in $\text{SiO}_2@\text{OPW}$ and interactions of Pb^{2+} ions with functional binding sites of $\text{SiO}_2@\text{OPW}$. Also, an intense signal occurs at 757 cm^{-1} due to Si—O—Si stretching vibrations

(Park et al., 2002). Further intensity of absorption peaks in $\text{SiO}_2@\text{OPW}$ is lesser due to coating of SiO_2 nanospheres over OPW surface. In Fig. 1c, absorption peaks at $\sim 2900\text{ cm}^{-1}$ and 1045 cm^{-1} are vanishing, which indicates the role of C—H and C—OH bonds in adsorption mechanism. New absorption peaks arise at 466 cm^{-1} , 687 cm^{-1} indicate Pb—O and Pb—O—Pb stretching vibrations respectively, which confirms the adsorption of Pb^{2+} ions onto the $\text{SiO}_2@\text{OPW}$ surface (Arulmozhi et al., 2013).

X-ray spectrum of OPW did not display any distinct peaks at any region. OPW contains completely organic materials having the amorphous nature (Fig. 2a). The broadband at $2\theta = 20\text{--}30^\circ$ in Fig. 2b, is attributed to the incorporation of amorphous silica into OPW surface. The diffraction peaks observed at $2\theta = 30.8^\circ$, 36.6° and 51.8° corresponds to diffraction planes (1 1 1), (2 0 0) and (2 2 0) respectively in the X-ray spectrum of Pb loaded $\text{SiO}_2@\text{OPW}$ (Fig. 2c) (Theivasanthi and Alagar, 2013). SEM analysis was done to identify the surface texture and morphology of OPW and $\text{SiO}_2@\text{OPW}$ nanocomposites. The result of SEM analysis is shown in Fig. 3(a)–(f). It can be clearly seen from Fig. 3a that OPW surface is rippled paper like smooth, compact sheet before chemical modification. Fig. 3b shows aggregate spherical silica nanoparticles. Their average particle size distribution is about $12\text{--}50\text{ nm}$. Of course, an obvious agglomeration of silica nanoparticles is observed due to three dimensional hydrophilic networks of $\text{—Si(OH)}_2\text{—O—Si(OH)}_2\text{—}$ groups onto silica water interface. Aggregate silica nanoparticles distributed on to the surface of the OPW sheet as shown in Fig. 3c and d. Moreover SiO_2 nanospheres completely covered the wrinkled paper like sheet of the OPW and provides different functional binding sites (—Si—O—Si— , Si—O^-) for adsorption of Pb^{2+} ions (Fig. 3e and f) (Saini et al., 2018). Fig. 4(a)–(d) gives the

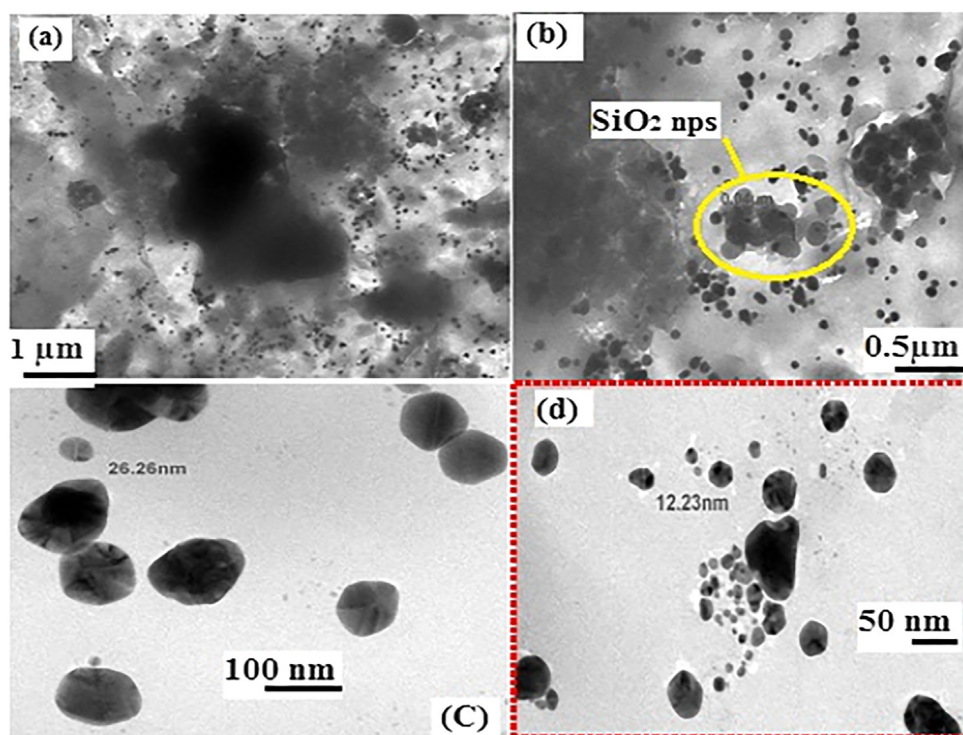


Fig. 4 (a–d) TEM images of $\text{SiO}_2@\text{OPW}$.

corresponding TEM images of $\text{SiO}_2@\text{OPW}$ nanospheres. These images also confirmed the spherical shape of silica nanoparticles and their continuous entrapping into the OPW surface (Fig. 4a and b). The average particle size of $\text{SiO}_2@\text{OPW}$ nanocomposites is about 26–200 nm as shown in TEM images.

EDX analysis has been done to find out the elemental composition of OPW, $\text{SiO}_2@\text{OPW}$ and Pb loaded $\text{SiO}_2@\text{OPW}$ before and after adsorption of Pb^{2+} ions. The weight percent of the detected elements in OPW is C 66.88, O 35.85, Si 0.62 and some additional peaks of copper and silver also appears (Fig. 5a). The weight percent of C 54.79, O 35.58 and Si 9.27 in $\text{SiO}_2@\text{OPW}$ is evident from Fig. 5b. Further weight percent of C 56.19, O 35.58, Si 1.27 and Pb 5.38 is observed in the EDX spectrum of Pb^{2+} loaded $\text{SiO}_2@\text{OPW}$ indicates adsorption of Pb^{2+} ions. Meanwhile, decrease in peak intensity of silica indicates participation of functional binding sites of silica in the adsorption mechanism (Fig. 5c).

3.1.1. Mechanism of adsorption

Uptake of Pb^{2+} ions onto $\text{SiO}_2@\text{OPW}$ is understood in terms of (a) Colloidal suspension surface charge; (b) Surface complexation of Pb^{2+} with different functional groups like

COOH , OH and $\text{C}=\text{O}$ present into pectin, lignin and cellulose of OPW; (c) Surface precipitation and physical adsorption. COO^- sites present in pectin creates chelation with Pb^{2+} ions. COOH and $\text{O}-\text{H}$ groups are involved in ion exchange between Pb^{2+} and O^- sites. Polymeric chains of silica hydrogel produce three dimensional network of $-\text{Si}(\text{OH})_2-\text{O}-\text{Si}(\text{OH})_2-$ groups onto silica water interface. This three dimensional network of $\text{Si}(\text{OH})_2-\text{O}-\text{Si}(\text{OH})_2$ is hydrophilic and capable of holding a large number of $[\text{SiO}^-]$ sites. Colloidal interactions of silica hydrogel are primarily strong vander wall interactions with the adsorbate species. These additional anionic binding sites introduce electrostatic attractions between Pb^{2+} , $[\text{Si}-\text{O}^-]$ and $[-\text{Si}-\text{O}-\text{Si}-]$. In addition, Pb^{2+} is co-precipitated as $\text{Pb}(\text{OH})_2$, $\text{Pb}(\text{CO}_3)_2$ and $\text{Pb}(\text{SiO}_3)_2$ in alkaline metallic solution. Meanwhile, decrease in peak intensity of silica (9.27–1.27) in the EDX spectrum of Pb^{2+} loaded $\text{SiO}_2@\text{OPW}$ confirms participation of functional binding sites of silica in the adsorption of Pb^{2+} (Mei et al., 2015; Yang et al., 2015; Shao et al., 2012). All possible interactions of Pb^{2+} onto $\text{SiO}_2@\text{OPW}$ are schematically illustrated in Scheme 1.

3.2. Adsorption experiment

3.2.1. Effect of pH

The affinity of adsorbent functional sites for metallic ions depends on the initial pH of the adsorbate solution. Lead occurs as Pb^{2+} , $\text{Pb}(\text{OH})^+$ and $\text{Pb}(\text{OH})_2$ species in deionized water. Typically, Pb^{2+} ions exist in the 6.5 pH solution, afterward, in the pH range from 6.5 to 9.0 exist as $\text{Pb}(\text{OH})^+$. The effect of pH on adsorption of Pb^{2+} ions was studied over a pH range of 2.0–8.0. The adsorption capacity for Pb^{2+} ions of both the adsorbents increased sharply from pH 2 to 6. Further the adsorption of Pb^{2+} reduced below pH 2.0 and above pH 6.0. Precipitation occurs at higher pH as Pb^{2+} ions precipitate as $\text{Pb}(\text{OH})^+$, $\text{Pb}(\text{OH})_2$, and $\text{Pb}(\text{OH})_3$. The Similar observations have been reported for the adsorption of Pb^{2+} ions by other authors (Kumar et al., 2014; Miranda et al., 2016).

Actually, in acidic solutions too H^+ ions concentration is not significant for replacement of Pb^{2+} ions is being attributed to competitive adsorption between proton and Pb^{2+} ions for occupying active sites onto OPW and $\text{SiO}_2@\text{OPW}$. May be functional groups on the adsorbents protonated and caused electrostatic repulsion for Pb^{2+} ions (Kataria and Garg, 2018). In the alkaline range electrostatic attractions occur between cationic Pb^{2+} ions and anionic adsorbent surface. This may be attributed to the deprotonation of functional groups like carboxylic (COOH) as COO^- , alcohols and phenols (OH) as O^- and SiOH as $\text{Si}-\text{O}^-$ at higher pH. The percent removal of Pb^{2+} increased from 21.82% to 88.22% by OPW and 26.58% to 95.86% by $\text{SiO}_2@\text{OPW}$ (Fig. 6a).

3.2.2. Effect of adsorbent dose on Pb^{2+} adsorption

The influence of adsorbent dose on the removal of Pb^{2+} was studied by varying the adsorbent dose from 0.01 g/50 mL to 0.03 g/50 mL. Percent removal of Pb^{2+} increased from 62.76% to 88.96%, 68.82% to 98.02% respectively onto OPW and $\text{SiO}_2@\text{OPW}$ with an increase in adsorbent dose (Fig. 6b). This may be due to increase in adsorption sites and surface area due to increase in adsorbent dose. These results for Pb^{2+} ion removal are in agreement with the findings of other authors (Miranda et al., 2016; Ay et al., 2017; Saini

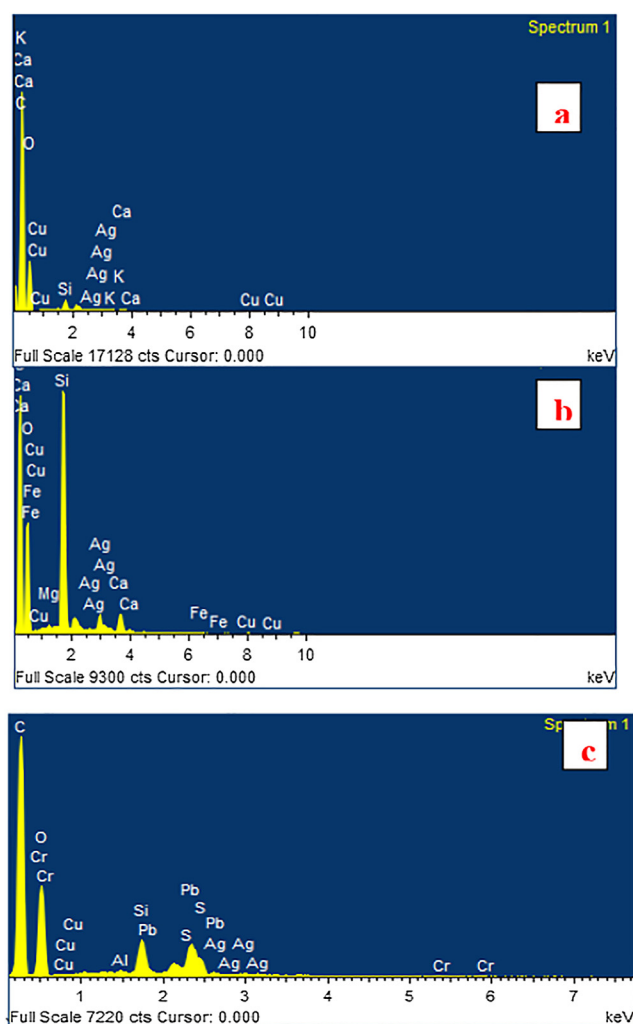
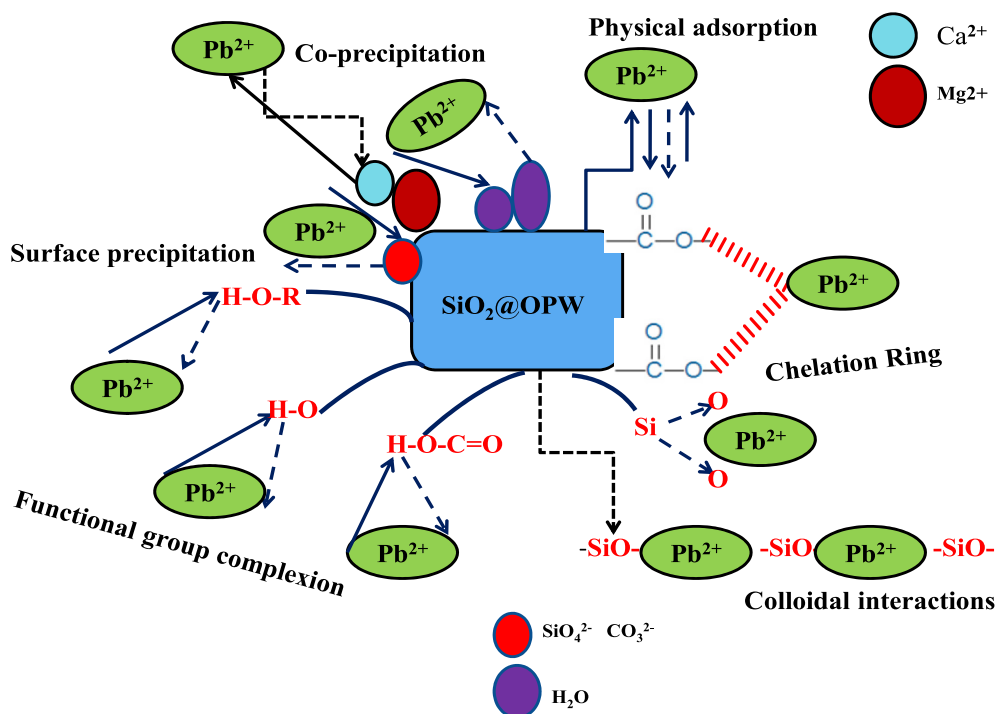


Fig. 5 (a–c) EDX of OPW, $\text{SiO}_2@\text{OPW}$ and Pb loaded $\text{SiO}_2@\text{OPW}$.



Scheme 1 Possible interactions between $\text{SiO}_2\text{@OPW}$ and Pb^{2+} ions.

et al., 2017). On the other hand, the adsorption capacity of OPW and $\text{SiO}_2\text{@OPW}$ decreased from 156.90 to 74.13 mg/g and 172.05 to 81.68 mg/g respectively with increase in the adsorbent dose. $\text{SiO}_2\text{@OPW}$ has more adsorption capacity than OPW that may be due to availability of more functional binding sites on the $\text{SiO}_2\text{@OPW}$ surface.

3.2.3. Effect of contact time and Pb^{2+} concentration on Pb^{2+} adsorption

The effect of contact time and Pb^{2+} concentration is depicted in Fig. 7. The experiments were performed by varying contact time (10–60 min.) and initial Pb^{2+} concentration (10–100 mg/L) keeping all other parameters constant. The percent removal increased from 58.68% to 87.88% onto OPW and 63.43% to 93.94% onto $\text{SiO}_2\text{@OPW}$ with time. Herein, the adsorption capacities of OPW increased from 22.03 to 147.38 mg/g and adsorption capacity of $\text{SiO}_2\text{@OPW}$ increased 24.92 to 197.93 mg/g as the initial concentration of Pb^{2+} ions increased from 10 to 100 mg/g. These results suggested that the actual amount of Pb^{2+} ions adsorbed per unit mass of the adsorbent increased with metal ion concentration (Ay et al., 2017; Ilangovan et al., 2017; Luo et al., 2016).

3.2.4. Effect of temperature on Pb^{2+} adsorption

The effect of temperature on the adsorption of Pb^{2+} was studied by varying temperature in the range of 10–50 °C. The Pb^{2+} adsorption increased from 43.98% to 93.94% onto OPW and 52.72% to 97.36% onto $\text{SiO}_2\text{@OPW}$ with increase in temperature (Fig. 8). The adsorption capacities also increased from 54.98 to 117.43 mg/g and 65.9 to 121.7 mg/g onto OPW and $\text{SiO}_2\text{@OPW}$ respectively. This may be due to increased mobility of ions with rise in temperature and increase in the number

of adsorptive sites due to adsorbent rupture at higher temperature. The adsorption of Pb^{2+} ions may be endothermic in nature as the adsorption percentage increased with temperature (Lawal et al., 2017; Luo et al., 2016).

3.3. Equilibrium isotherms

To better analyze the equilibrium relationship between Pb^{2+} and $\text{SiO}_2\text{@OPW}$, the equilibrium data was modeled by two common models, viz., the Langmuir isotherm model and the Freundlich isotherm model. These adsorption isotherms provide the adsorption capacity of adsorbents in order to choose the efficient adsorbents for water treatment and also to compare the adsorption capacities of various adsorbents. The Langmuir equilibrium isotherm model assumes monolayer distribution of metal ion concentration at specific homogeneous sites within the adsorbent surface and no interaction between adsorbed species. While the Freundlich isotherm model describes that adsorption happens on the heterogeneous surface system. The isotherm model provides the relationship between the amount of adsorbate adsorbed per unit mass of the adsorbent and concentration of adsorbate at equilibrium.

Linear forms of Langmuir and Freundlich isotherm are given in Eqs. (3) and (4) respectively (Langmuir, 1918; Freundlich, 1906).

$$\frac{C_e}{q_e} = \frac{1}{q_{\max}b} + \frac{C_e}{q_{\max}} \quad (3)$$

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \quad (4)$$

where $q_{\max}$ (mg/g) is the maximum adsorption capacity at monolayer coverage, b (L/mg) is the Langmuir constant

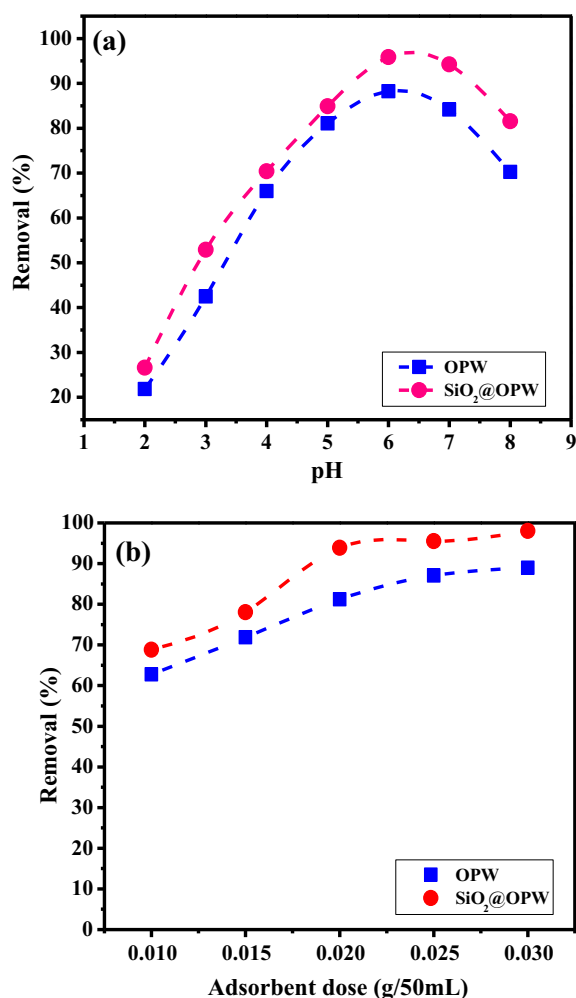


Fig. 6 (a) Effect of pH on adsorption of Pb²⁺ ions onto OPW and SiO₂@OPW (Experimental Conditions: Pb²⁺ conc. – 50 mg/L, adsorbent dose – 0.02g/50mL, temp. – 27 °C, contact time – 1 h). (b) Effect of adsorbent dose on adsorption of Pb²⁺ ions onto OPW and SiO₂@OPW nanocomposites. (Experimental Conditions: pH – 6, Pb²⁺ ions conc. – 50 mg/L, temp. – 27 °C, contact time – 1 h).

parameter related to the energy of adsorption and affinity of binding sites between adsorbate and adsorbent. K_f is Freundlich constant. The constant n , is the heterogeneity factor related to the intensity and favorability of the adsorption. The value of q_{max} (mg/g), b (L/mg) and correlation coefficient (R^2) are determined from a plot of C_e/q_e vs C_e (Fig. 9a and b). The constant K_f , R^2 and n are calculated from the slope and intercept of the plot between $\log q_e$ and $\log C_e$ (Fig. 10a and b). The values of n should lie in between 1 and 10 for favourable adsorption. All the calculated parameters are listed in Table 2.

Here, the value of the correlation coefficient R^2 for Langmuir isotherm was (0.999) for both OPW and SiO₂@OPW and the adsorption capacity was 166.6 mg/g, 200.0 mg/g onto OPW and SiO₂@OPW which is much closer to the experimental results i. e. 147.37 mg/g and 197.93 mg/g. The value of coefficient R^2 was 0.952 and 0.929 for OPW and SiO₂@OPW as

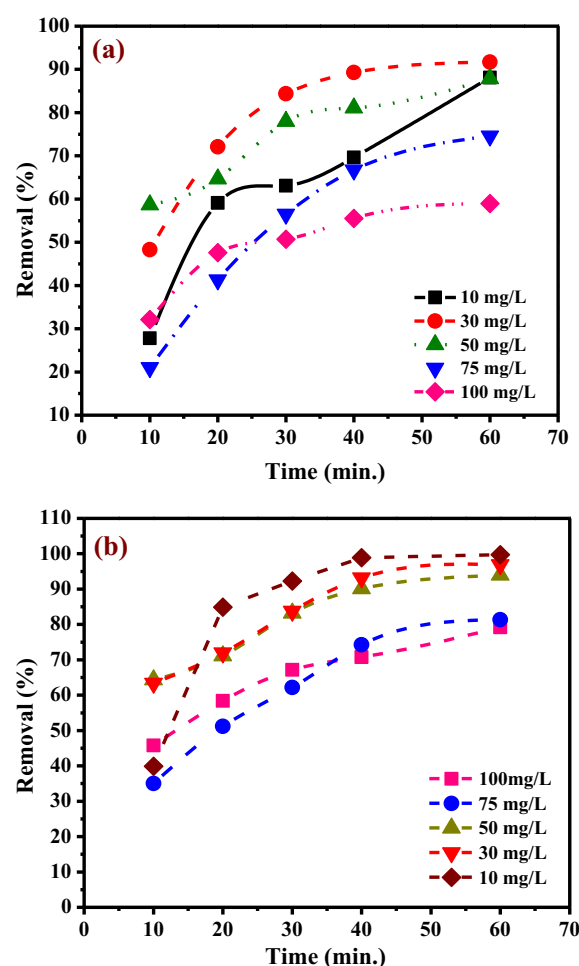


Fig. 7 (a) Effect of metal ion concentration and contact time on Pb²⁺ adsorption onto OPW (b) Onto SiO₂@OPW. (Experimental Conditions: Pb²⁺ ion conc.: 10–100 mg/L, temp.: 27 °C, contact time: 1 h, pH: 6.0).

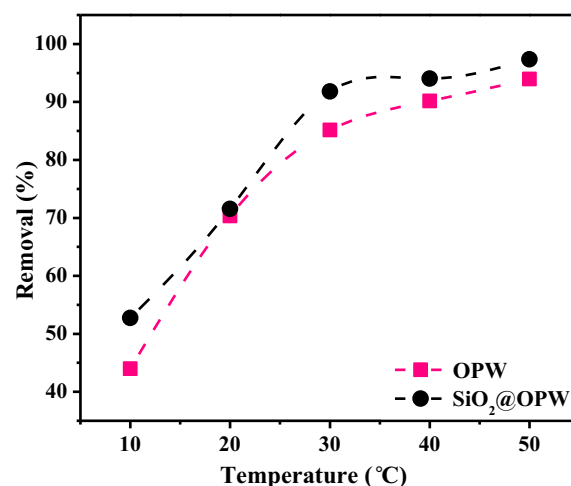


Fig. 8 Effect of temperature on the adsorption of Pb²⁺ ions onto OPW and SiO₂@OPW. (Experimental Conditions: pH – 6, metal ion conc. – 50 mg/L, dose – 0.02 g/50 mL, contact time – 1 h).

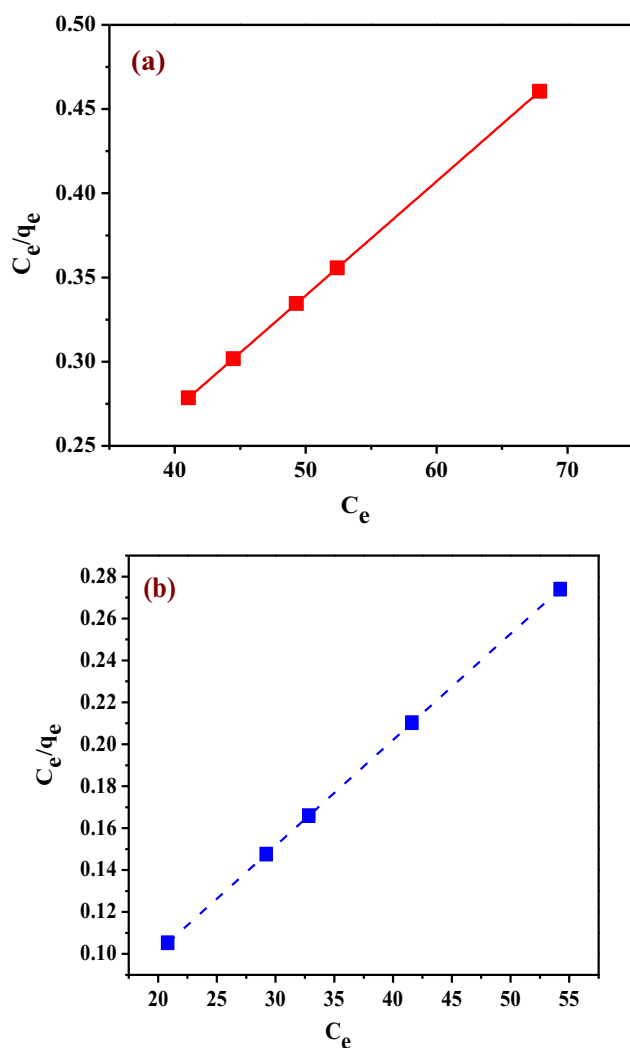


Fig. 9 Langmuir adsorption isotherms plots for Pb^{2+} ions onto OPW and $\text{SiO}_2\text{@OPW}$ (a) OPW, (b) $\text{SiO}_2\text{@OPW}$.

obtained from Freundlich isotherm. In comparison to Freundlich isotherm, owing to high values of correlation coefficients and adsorption capacities the Langmuir isotherm fits better with the experimental data for Pb^{2+} adsorption onto $\text{SiO}_2\text{@OPW}$. The calculated adsorption capacity was much higher than the other previously reported studies [Table 3].

3.4. Adsorption kinetics

To investigate the rate mechanism the, experimental data was evaluated by pseudo-first order, pseudo-second order and intraparticle diffusion equations given as Eqs. (5–7) respectively (Lagergren, 1898; Ho and McKay, 1999; Weber and Morris, 1963).

$$\log(q_e - q_t) = \log q_e - \left(\frac{k_1}{2.303} \right) t \quad (5)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (6)$$

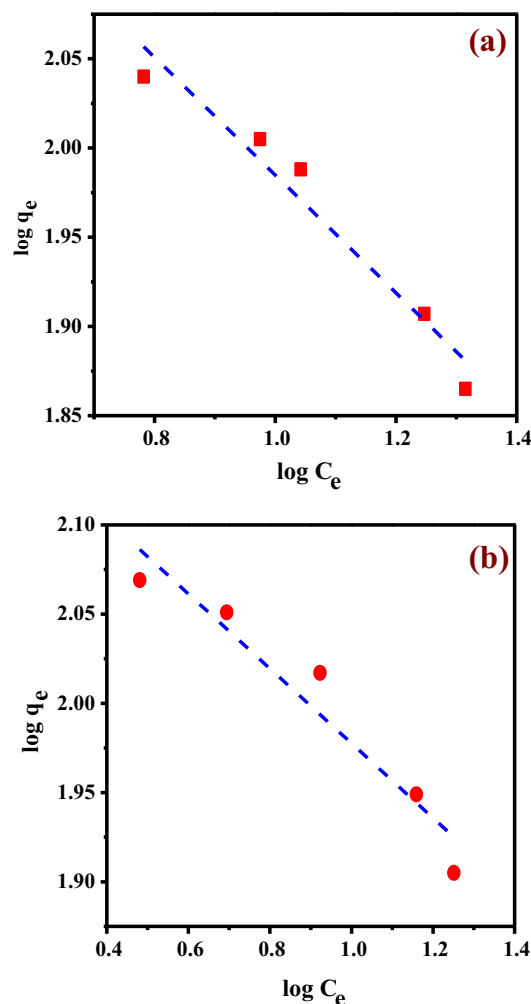


Fig. 10 Freundlich adsorption isotherm plot for Pb^{2+} metal ions onto OPW and $\text{SiO}_2\text{@OPW}$ (a) OPW, (b) $\text{SiO}_2\text{@OPW}$

$$q_t = k_{id} t^{1/2} + C \quad (7)$$

where q_e and q_t (mg/g) are the amount of Pb^{2+} adsorbed per unit mass of the adsorbent at any time t and equilibrium time, respectively, k_1 (min^{-1}) and k_2 ($\text{g mg}^{-1} \text{min}^{-1}$) are the pseudo-first order and pseudo-second order rate constants, k_{id} is the intraparticle diffusion rate constant and C is intercept which provides an approximation about the thickness of the boundary layer. k_1 and q_e is calculated from the slope and intercept of a linear plot between $\log(q_e - q_t)$ and t (Figs. 11 and 12a). The equilibrium capacity, q_e and k_2 is determined from the slope and intercept of the plot between t/q_t versus t as shown in Figs. 11 and 12b. The value of C and k_{id} can be obtained by the slope and intercept of the plot between $t^{1/2}$ versus q_t (Figs. 11 and 12c). The calculated parameters were listed in Table 1.

A better straight line fitting, correlation coefficient R^2 (>0.999) is obtained for both OPW and $\text{SiO}_2\text{@OPW}$ from pseudo-second order equation. Meanwhile the calculated q_e values are in good agreement with experimental q_e values. These results confirmed the well fitting of Pseudo-second-order equation for the adsorption of Pb^{2+} onto $\text{SiO}_2\text{@OPW}$.

Table 1 Kinetic models parameters study for Pb^{2+} ion uptake onto OPW and $SiO_2@OPW$.

Kinetic models parameters		Values of parameters			
		OPW		$SiO_2@OPW$	
		50 mg/L	100 mg/L	50 mg/L	100 mg/L
Pseudo-first order	k_1 (min^{-1})	0.071	0.080	0.085	0.073
	q_e (cal)	0.304	0.351	0.394	0.305
	R^2	0.953	0.972	0.904	0.978
Pseudo-second order	k_2 (g/mg min)	0.0004	0.0009	0.00033	0.00081
	q_e (cal)	125.0	200.0	142.85	250.0
	R^2	0.994	0.997	0.995	0.997
Intraparticle diffusion	k_{id} ($\text{mg g}^{-1} \text{min}^{-1/2}$)	9.63	16.33	10.08	20.58
	C	41.48	35.87	47.23	51.50
	R^2	0.969	0.936	0.980	0.988
Experimental data	q_e (exp)	109.85	147.37	117.43	197.0

Intraparticle diffusion plot uptake is linear, which indicates its participation in the adsorption kinetics of Pb^{2+} onto $SiO_2@OPW$ (Zhu et al., 2018). Although, it did not pass through the origin, confirms not only intraparticle diffusion is a rate limiting step but other kinetic models also. Based

on that interpretation, adsorption of Pb^{2+} ions onto $SiO_2@OPW$ is a complex diffusion process involving both boundary layer diffusion and intraparticle diffusion.

3.4.1. Desorption and reuse potential of $SiO_2@OPW$

Adsorbed Pb^{2+} ions were removed from metal laden $SiO_2@OPW$ using hydrochloric acid of various strengths ranging from 0.1 to 0.3 M. 0.03 g of metal amalgamated $SiO_2@OPW$ were added to 20 mL of HCl of desired concentration and agitated for 60 min in a closed shaker. Desorption efficiency was increased from 48.3% to 82.5% with increasing HCl concentration. Existence of H^+ sites at lower pH favours the regeneration of $SiO_2@OPW$. However an optimum was achieved at 0.025 M, further on desorption efficiency remained constant. Five adsorption-desorption cycles were evaluated to determine the reuse potential of $SiO_2@OPW$. The results showed that $SiO_2@OPW$ nanoadsorbents had good removal efficiency (80.16–85.62%) upto three cycles. The removal efficiency was ~68.9% during 4th and 5th cycle (Fig. 13).

Table 2 Adsorption isotherms model parameters for Pb^{2+} ions uptake onto OPW and $SiO_2@OPW$.

Isotherms model	Parameters	Parameters values	
		OPW	$SiO_2@OPW$
Langmuir	q_{max} (mg/g)	166.6	200
	b (L/mg)	0.006	0.005
	R^2	0.999	0.999
Freundlich	$1/n$	3.03	4.78
	K_f (mg/g)	2.314	2.186
	R^2	0.953	0.929

Table 3 Adsorption capacity of various adsorbents for Pb^{2+} ion.

Adsorbent	q_{max} (mg/g)	Reference
Nitrogen functionalized mesoporous Carbon	80.42	Yang et al. (2014)
Nanocomposite of ZnO with Montmorillonite	88.05	Sani et al. (2018)
Ethylenediamine-modified yeast biomass mixed matrix membrane	121.26	Li et al. (2013)
Polysulfone/hydrous ferric oxide	13.20	Abdullah et al. (2016)
Mixed membrane		
Activated carbon prepared from rapeseed oil	133.8	Erdem et al. (2015)
Graphene oxide-hydrated manganese oxide nanocomposites	500.0	Wan et al. (2016)
Magnetic cellulose nanocomposite beads entrapping activated bentonite	12.6	Luo et al. (2016)
Black walnut (<i>Juglan nigra</i>) husk	3.0	Lawal et al. (2017)
	115	
Nanoscale zero valent supported by Zeolite and Montmorillonite	115 and 50.3	Miranda et al. (2016)
Pine cone activated carbon	27.53	Momcilovic et al. (2011)
OPW	166.6	Present work
$SiO_2@OPW$	200.0	Present work

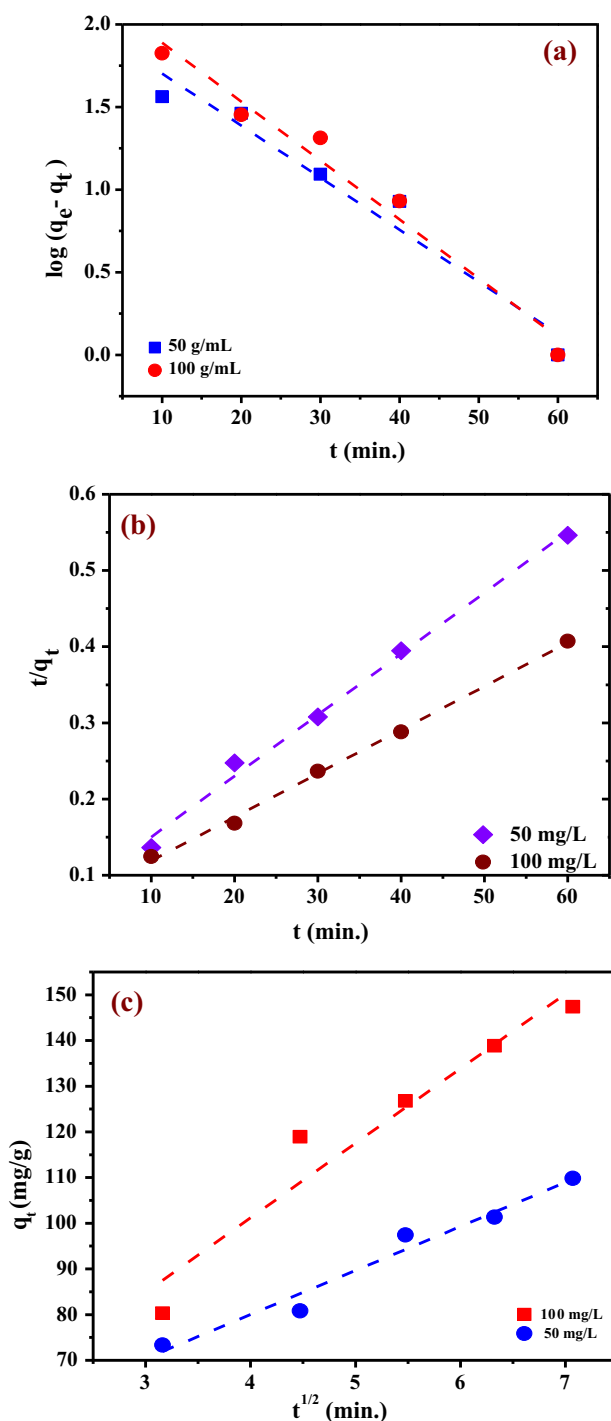


Fig. 11 Kinetic plots for adsorption for Pb^{2+} metal ions onto OPW. (a) Pseudo-first-order plot, (b) pseudo-second order plot, (c) intraparticle diffusion plot.

4. Conclusion

A novel adsorbent, SiO_2 functionalized orange peel waste ($\text{SiO}_2@\text{OPW}$) has been prepared, characterized & tested for Pb^{2+} adsorption from aqueous medium to explore its potential in wastewater treatment. The dispersion of SiO_2 onto the surface of OPW is confirmed by XRD, FTIR, SEM and

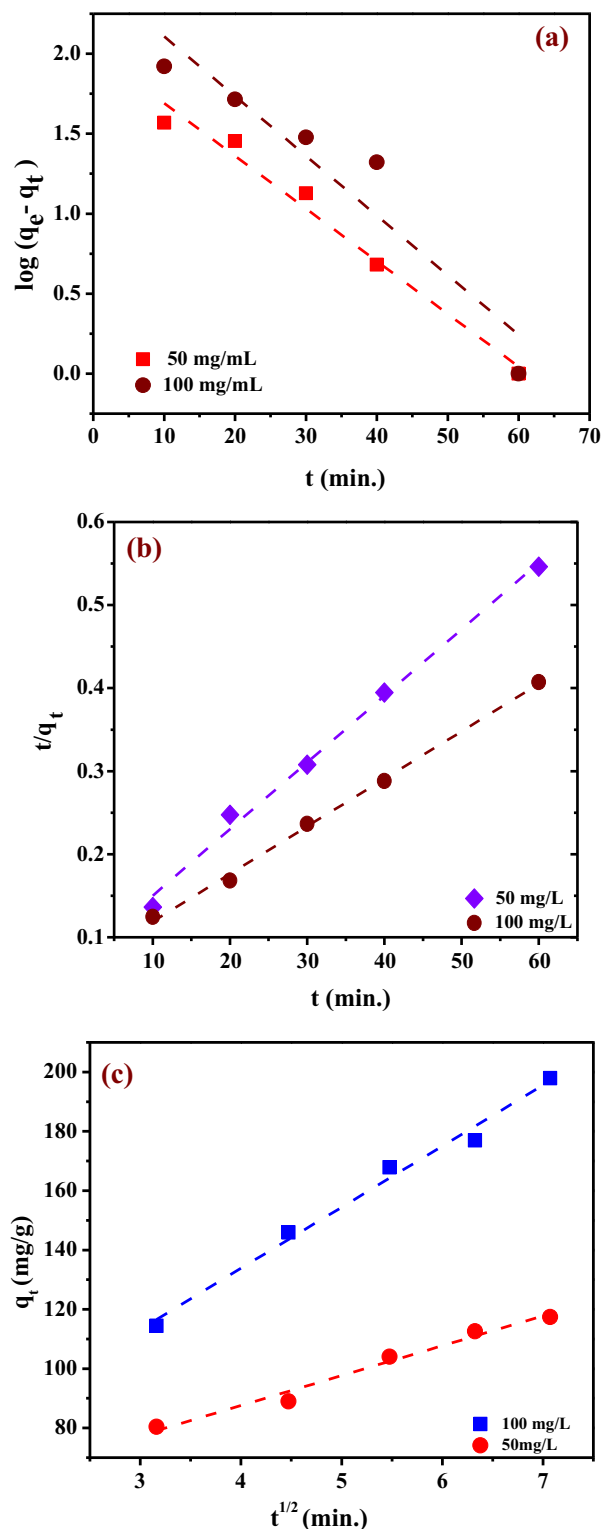


Fig. 12 Kinetic plots for adsorption for $\text{Pb}(\text{II})$ metal ions onto $\text{SiO}_2@\text{OPW}$. (a) Pseudo-first-order plot, (b) pseudo-second order plot, (c) intraparticle diffusion plot.

TEM images. $\text{SiO}_2@\text{OPW}$ has enhanced adsorption capacity for Pb^{2+} ions as compared to pristine orange peel waste. Increase in adsorption capacity of $\text{SiO}_2@\text{OPW}$ may be attributed to new electrostatic interactions between Pb^{2+} , $\text{Si}-\text{O}^-$

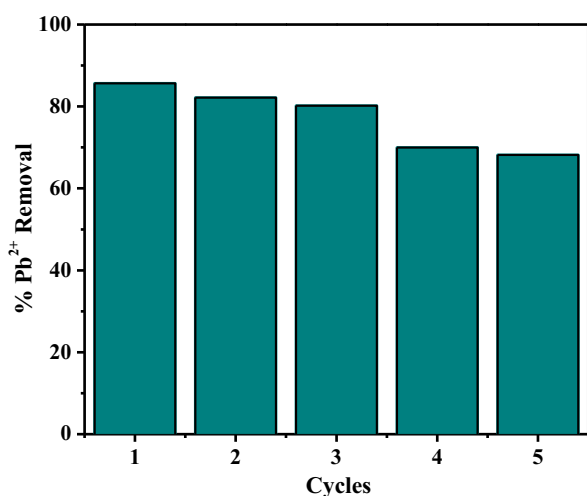


Fig. 13 Efficiency of SiO₂@ OPW for Pb²⁺ removal during adsorption-desorption cycles.

and —Si—O—Si— functional binding sites of SiO₂ nanospheres entrapped onto the OPW. The optimum adsorbent dosage was 0.02 g/L at pH = 6. The maximum monolayer adsorption capacity calculated from Langmuir isotherm model was 166.6 mg/g, 200.0 mg/g for OPW and SiO₂@OPW respectively. The kinetic data fitted well to the pseudo-second-order and intraparticle diffusion models.

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